

**ACRYLIC COPOLYMER COMPOSITION, METHOD FOR  
PREPARING ACRYLIC COPOLYMER, AND VINYL CHLORIDE  
RESIN COMPOSITION CONTAINING THE ACRYLIC COPOLYMER**

**5        Technical Field**

The present invention relates to an acrylic copolymer composition, a method for preparing an acrylic copolymer, and a vinyl chloride resin composition containing the acrylic copolymer. More particularly, the present  
10 invention relates to an acrylic copolymer which improves the foamability of a vinyl chloride resin such as polyvinyl chloride (PVC) when used as an additive for the vinyl chloride resin and further improves the impact strength of the vinyl chloride resin when used in combination with an  
15 impact modifier, and a vinyl chloride resin composition containing the same.

**Background Art**

Vinyl chloride resins are polymers containing 50% or  
20 more of vinyl chloride. Since the vinyl chloride resins are inexpensive, are easy in hardness adjustment, and can be applied in most processing machines, they have various application fields. In addition, the vinyl chloride resins can be processed into formed products with good physical  
25 and chemical properties, and thus, are widely used in

various fields.

However, the vinyl chloride resins have many disadvantages in impact strength, processability, thermal stability, and heat deflection temperature. In this  
5 respect, additives for solving these disadvantages have been developed and used. Examples of additives for the vinyl chloride resins include impact modifiers, processing aids, stabilizers, and fillers, and are selectively used according to their purposes.

10 Recently, there has been an increasing interest in a foam-forming process to decrease the mass of vinyl chloride resins and costs of formed products. However, foam-forming of only vinyl chloride resins cannot provide a sufficient elongation and melt strength, which causes poor appearance  
15 of formed products and low expansion ratio due to large and non-uniform foamed cells. To solve these problems, addition of a mixture of a processing aid containing methyl methacrylate as a main component and a blowing agent to a vinyl chloride resin is generally used.

20 U.S. Patent No. 6,140,417 discloses a vinyl chloride resin composition including a vinyl chloride resin and a processing aid for imparting improved processability and foamability to the vinyl chloride resin. The processing aid is prepared by three-stage polymerization of a compound  
25 selected from methyl methacrylate, alkyl acrylate, and

alkyl methacrylate, and a copolymerizable vinyl monomer. The three-stage polymerization includes a first stage polymerization for a low glass transition temperature ( $T_g$ ), a second stage polymerization for a higher  $T_g$  than the first stage polymerization, and a third stage polymerization for a lower  $T_g$  than the second stage polymerization. U.S. Patent No. 6,221,966 discloses a vinyl chloride resin composition including a vinyl chloride resin and a processing aid prepared by two-stage polymerization to impart improved processability, transparency, and foamability to the vinyl chloride resin. The processing aid has a small particle size, its inner layer contains a small amount of methyl methacrylate for low  $T_g$ , and its outer layer contains a large amount of methyl methacrylate for high  $T_g$ . However, these vinyl chloride resin compositions are insufficient in terms of enhancement of processability and uniformity of foamed cells.

U.S. Patent No. 6,391,976 discloses a vinyl chloride resin composition including a small quantity of a processing aid composed of methyl methacrylate and alkyl methacrylate of 3-5 carbon atoms. However, processability and foamability are insufficient.

In addition, there have been studies about combination of functions of several additives used to

overcome many disadvantages of vinyl chloride resins, i.e., multi-purpose additives. Recently, in particular, studies about additives having combined characteristics of an impact modifier and a processing aid have been done. By way of example, European Patent No. EP 1,111,001 discloses a method for improving the impact strength of a vinyl chloride resin by adding powder particles composed of impact modifier particles and processing aid particles to the vinyl chloride resin, in which the powder particles are prepared by mixing an impact modifier and a processing aid in a latex phase, followed by coagulation and drying. However, this method is restrictive since latex mixing is required. Furthermore, this method is silent about information about formation of foamed products, and thus, a sufficient impact strength is not ensured.

#### Disclosure of Invention

In view of these problems, the present invention provides an acrylic copolymer composition which improves the foamability of a vinyl chloride resin when used as an additive for the vinyl chloride resin and further improves the impact strength of the vinyl chloride resin when used in combination with an impact modifier.

The present invention also provides a vinyl chloride resin composition containing an acrylic copolymer prepared

from the acrylic copolymer composition, which is excellent in foamability.

The present invention also provides a vinyl chloride resin composition containing an acrylic copolymer prepared  
5 from the acrylic copolymer composition and an impact modifier, which is excellent in impact strength.

According to an aspect of the present invention, there is provided an acrylic copolymer composition including: (A) 5-15 wt% of a crosslinking agent and an  
10 alkyl acrylate monomer constituting an alkyl acrylate crosslinked polymer; (B) 55-90 wt% of methyl methacrylate; and (C) 5-40 wt% of at least one monomer selected from the group consisting of an alkyl acrylate compound and an alkyl methacrylate compound.

15 The degree of swelling of the alkyl acrylate crosslinked polymer may be in a range of 3 to 10.

The alkyl acrylate monomer constituting the alkyl acrylate crosslinked polymer may be an alkyl acrylate compound and the alkyl acrylate crosslinked polymer may be  
20 prepared from the crosslinking agent and the alkyl acrylate compound.

The crosslinking agent may be selected from the group consisting of aryl methacrylate, trimethylolpropane, triacrylate, and divinylbenzene.

25 The alkyl acrylate compound constituting the alkyl

acrylate crosslinked polymer may have a straight, branched, or cyclic alkyl group of 1-18 carbon atoms.

The alkyl acrylate compound constituting the alkyl acrylate crosslinked polymer may be one or more selected  
5 from the group consisting of methyl acrylate, ethyl acrylate, n-butyl acrylate, lauryl acrylate, stearyl acrylate, 2-ethylhexyl acrylate, and cyclohexyl acrylate.

The alkyl acrylate compound of the monomer (C) may have a straight, branched, or cyclic alkyl group of 1-18  
10 carbon atoms and the alkyl methacrylate compound of the monomer (C) may have a straight or cyclic alkyl group of 2-18 carbon atoms.

The alkyl acrylate compound of the monomer (C) may be one or more selected from the group consisting of methyl  
15 acrylate, ethyl acrylate, n-butyl acrylate, lauryl acrylate, stearyl acrylate, 2-ethylhexyl acrylate, and cyclohexyl acrylate. The alkyl methacrylate compound of the monomer (C) may be one or more selected from the group consisting of n-butyl methacrylate, lauryl methacrylate, stearyl  
20 methacrylate, tridecyl methacrylate, i-butyl methacrylate, t-butyl methacrylate, 2-ethylhexyl methacrylate, and cyclohexyl methacrylate.

The acrylic copolymer may have a weight average molecular weight of 1,000,000 to 12,000,000.

25 According to another aspect of the present invention,

there is provided a method for preparing an acrylic copolymer, which includes emulsion polymerization, suspension polymerization, or solution polymerization of 5-15 wt% of a crosslinking agent and an alkyl acrylate monomer constituting an alkyl acrylate crosslinked polymer having the degree of swelling of 3 to 10; 55-90 wt% of methyl methacrylate; and 5-40 wt% of at least one monomer selected from the group consisting of an alkyl acrylate compound and an alkyl methacrylate compound.

10 The emulsion polymerization preparing an acrylic copolymer may include (a) (i) mixing 5-15 wt% of the crosslinking agent and the alkyl acrylate monomer to prepare an emulsion containing the alkyl acrylate crosslinked polymer having the degree of swelling of 3 to 10 and adding 27.5-45 wt% of the methyl methacrylate, 2.5-20 wt% of the at least one monomer selected from the group consisting of the alkyl acrylate compound with an alkyl group of 1-18 carbon atoms and the alkyl methacrylate compound with an alkyl group of 2-18 carbon atoms, an emulsifier, a polymerization initiator, and a redox catalyst, to the emulsion containing the alkyl acrylate crosslinked polymer or (ii) mixing 27.5-45 wt% of the methyl methacrylate, 2.5-20 wt% of the at least one monomer selected from the group consisting of the alkyl acrylate compound and the alkyl methacrylate compound, the

emulsifier, the polymerization initiator, and the redox catalyst, and adding 5-15 wt% of the crosslinking agent and the alkyl acrylate monomer to the mixture; and (b) further adding 27.5-45 wt% of the methyl methacrylate, 2.5-20 wt%  
5 of the at least one monomer selected from the group consisting of the alkyl acrylate compound and the alkyl methacrylate compound, the emulsifier, the polymerization initiator, and the redox catalyst, to the resultant mixture of step (a).

10 According to another aspect of the present invention, there is provided a vinyl chloride resin composition including a vinyl chloride resin and 0.1-20 parts by weight of an acrylic copolymer prepared according to the method, based on 100 parts by weight of the vinyl chloride resin.

15 According to yet another aspect of the present invention, there is provided a vinyl chloride resin composition including a vinyl chloride resin and 1-30 parts by weight of a mixture comprising 5-30 wt% of an acrylic copolymer prepared according to the method and 70-95 wt% of  
20 an impact modifier, based on the 100 parts by weight of the vinyl chloride resin.

The impact modifier may be selected from the group consisting of acrylonitrile-butadiene-styrene (ABS), methyl methacrylate-butadiene-styrene (MBS), and acrylic compounds.

25 Hereinafter, the present invention will be described



in more detail.

An acrylic copolymer prepared from an acrylic copolymer composition including a specific crosslinked polymer and a non-crosslinked polymer in a predetermined ratio according to the present invention improves the foamability of a vinyl chloride resin when added to the vinyl chloride resin. Further, when a mixture of the acrylic copolymer and an impact modifier is used as an additive for the vinyl chloride resin, the vinyl chloride resin can have a higher impact strength, as compared to when the impact modifier is used alone.

That is, the acrylic copolymer composition of the present invention includes 5-15 wt% of a crosslinking agent and an alkyl acrylate monomer constituting an alkyl acrylate crosslinked polymer; and 55-90 wt% of methyl methacrylate and 5-40 wt% of at least one selected from the group consisting of an alkyl acrylate compound and an alkyl methacrylate compound constituting a non-crosslinked copolymer.

Preferably, the alkyl acrylate crosslinked polymer has the degree of swelling from 3 to 10 to lower its glass transition temperature. The alkyl acrylate crosslinked polymer serves to increase the degree of swelling of the acrylic copolymer of the present invention, thereby enhancing the swell characteristics, and is prepared from a

crosslinking agent and an alkyl acrylate compound. If the degree of swelling is less than 3, good die swell characteristics may not be obtained. On the other hand, if it exceeds 10, processability suitable for a vinyl chloride resin may not be ensured, which makes it difficult to produce a good foamed product.

Preferably, the crosslinking agent and the alkyl acrylate monomer constituting the alkyl acrylate crosslinked polymer are used in an amount of 5 to 15 wt%. If the content of the crosslinking agent and the alkyl acrylate monomer is less than 5 wt%, a formed product may have an insufficient expansion ratio. On the other hand, if it exceeds 15 wt%, fine and uniform foamed cells may not be obtained.

Preferably, the crosslinking agent is aryl methacrylate, trimethylolpropane, triacrylate, divinylbenzene, or the like.

Preferably, the alkyl acrylate compound constituting the alkyl acrylate crosslinked polymer has a straight, branched, or cyclic alkyl group of 1-18 carbon atoms. More preferably, the alkyl acrylate compound is methyl acrylate, ethyl acrylate, n-butyl acrylate, lauryl acrylate, stearyl acrylate, 2-ethylhexyl acrylate, or cyclohexyl acrylate.

Preferably, the methyl methacrylate constituting the non-crosslinked polymer is used in an amount of 55-90 wt%,

based on the total weight of the acrylic copolymer composition. If the content of the methyl methacrylate is less than 55 wt%, compatibility with a vinyl chloride resin may be lowered, thereby deteriorating processability. On the other hand, if it exceeds 90 wt%, dispersibility in a vinyl chloride resin composition may be lowered, thereby producing fish-eyes. More preferably, the methyl methacrylate is used in an amount of 70 to 80 wt%.

Preferably, the alkyl acrylate compound constituting the non-crosslinked copolymer has a straight, branched, or cyclic alkyl group of 1-18 carbon atoms and the alkyl methacrylate compound constituting the non-crosslinked copolymer has a straight or cyclic alkyl group of 2-18 carbon atoms. More preferably, the alkyl acrylate compound is methyl acrylate, ethyl acrylate, n-butyl acrylate, lauryl acrylate, stearyl acrylate, 2-ethylhexyl acrylate, or cyclohexyl acrylate, and the alkyl methacrylate compound is n-butyl methacrylate, lauryl methacrylate, stearyl methacrylate, tridecyl methacrylate, i-butyl methacrylate, t-butyl methacrylate, 2-ethylhexyl methacrylate, or cyclohexyl methacrylate.

Preferably, the weight average molecular weight of an acrylic copolymer, except a crosslinked polymer component, prepared from the above-described composition is in a range of 1,000,000 to 12,000,000.

A method for preparing an acrylic copolymer is not limited by polymerization methods. Preferably, emulsion polymerization, suspension polymerization or solution polymerization are used and the emulsion polymerization is more preferable.

That is, a method for preparing an acrylic copolymer by an emulsion polymerization according to the present invention may include (a) (i) mixing 5-15 wt% of a crosslinking agent and an alkyl acrylate monomer to prepare an emulsion containing an alkyl acrylate crosslinked polymer having the degree of swelling of 3 to 10 and adding 27.5-45 wt% of methyl methacrylate, 2.5-20 wt% of at least one monomer selected from the group consisting of an alkyl acrylate compound with an alkyl group of 1-18 carbon atoms and an alkyl methacrylate compound with an alkyl group of 2-18 carbon atoms, an emulsifier, a polymerization initiator, and a redox catalyst, to the emulsion containing the alkyl acrylate crosslinked polymer or (ii) mixing 27.5-45 wt% of the methyl methacrylate, 2.5-20 wt% of the at least one monomer selected from the group consisting of the alkyl acrylate compound with an alkyl group of 1-18 carbon atoms and the alkyl methacrylate compound with an alkyl group of 2-18 carbon atoms, the emulsifier, the polymerization initiator, and the redox catalyst, and adding 5-15 wt% of the crosslinking agent and the alkyl

acrylate monomer to the mixture; and (b) further adding 27.5-45 wt% of the methyl methacrylate, 2.5-20 wt% of the at least one monomer selected from the group consisting of the alkyl acrylate compound with an alkyl group of 1-18 carbon atoms and the alkyl methacrylate compound with an alkyl group of 2-18 carbon atoms, the emulsifier, the polymerization initiator, and the redox catalyst, to the resultant mixture of step (a).

Preferably, the emulsifier is used in an amount of 0.5 to 5 wt%, based on the total weight of all components used in the preparation of the acrylic copolymer. There are no particular limitations on the type of the emulsifier that can be used herein. However, it is preferable to use, as the emulsifier, an anionic emulsifier such as aliphatic ester, alkyl benzene sulfonate, alkyl phosphate, and dialkyl sulfosuccinate, and a non-ionic emulsifier such as polyoxyethylene alkyl ether and alkylamine ester, alone or in combination.

Preferably, the crosslinking agent is used in an amount of 0.01 to 0.3 wt%, based on the total weight of all components used in the preparation of the acrylic copolymer. The crosslinking agent may be aryl methacrylate, trimethylolpropane, triacrylate, or divinylbenzene. An acrylate compound is more preferable.

Preferably, the polymerization initiator is used in

an amount of 0.0005 to 0.005 wt%, based on the total weight of all components used in the preparation of the acrylic copolymer. The polymerization initiator may be a water-soluble initiator such as potassium persulfate, ammonium persulfate, and sodium persulfate, an oil-soluble initiator such as t-butyl hydroperoxide, cumene hydroperoxide, benzoyl peroxide, and lauryl peroxide, or a redox initiator.

Preferably, the redox catalyst is used in an amount of 0.01 to 0.1 wt%, based on the total weight of all components used in the preparation of the acrylic copolymer. The redox catalyst may be sodium formaldehydesulfoxylate, disodium ethylenediaminetetraacetate, sodium formaldehyde sulfoxylate, ferrous sulfate, sodium ethylenediaminetetraacetate, or cupric sulfate.

A latex acrylic copolymer prepared by the emulsion polymerization is converted to a powdery acrylic copolymer by coagulation, dehydration, and drying.

The acrylic copolymer prepared as described above can be contained in a vinyl chloride resin composition to impart good foamability to a vinyl chloride resin. Therefore, the present invention also provides a vinyl chloride resin composition including a vinyl chloride resin and 0.1 to 20 parts by weight of the acrylic copolymer, based on 100 parts by weight of the vinyl chloride resin.

A use of the acrylic copolymer within the above content

range can enhance a melt strength and a die swell property which are important factors for extrusion-foaming of the vinyl chloride resin, resulting in a foamed product which is excellent in foam density, expansion ratio, uniformity  
5 of foamed cells, and the like.

The present invention also provides a vinyl chloride resin composition including a vinyl chloride resin and 1-30 parts by weight of a mixture comprising 5-30 wt% of the acrylic copolymer and 70-95 wt% of an impact modifier,  
10 based on 100 parts by weight of the vinyl chloride resin. The combination of the acrylic copolymer of the present invention and the impact modifier can provide a higher impact strength, as compared to when the impact modifier is used alone, which makes it possible to produce a formed  
15 product with a sufficient impact strength.

Preferably, the impact modifier is acrylonitrile-butadiene-styrene (ABS), methyl methacrylate-butadiene-styrene (MBS), or an acrylic modifier. The acrylic modifier is more preferable in terms of weatherability of a  
20 formed product.

Hereinafter, the present invention will be described more specifically by Examples but the present invention is not limited to or by them.

25       Modes for Carrying Out the Invention

Examples 1-10 and Comparative Examples 1-7:Preparation of acrylic copolymers[Example 1](1) Preparation of acrylic copolymer

5        420 g of ion exchange water, 10 g of a 8% potassium salt solution of fatty acid, 59.5 g of butyl acrylate, and 0.5 g of aryl methacrylate were placed in a 3l four-necked flask reactor equipped with a stirrer, a thermocouple, a nitrogen inlet, and a reflux condenser, to prepare an  
10 emulsion. Then, the reactor was maintained at an internal temperature of 62°C under a nitrogen atmosphere and 0.45 g of t-butyl hydroperoxide (10% diluted solution) and 12 g of an activation solution were added to the reactor to perform a primary batch reaction. As the activation solution,  
15 there was used a mixture of 0.017 g of disodium ethylenediaminetetraacetate (EDTA), 0.04 g of sodium formaldehyde sulfoxylate (SFS), 0.001 g of ferrous sulfate, and 1.406 g of ion exchange water.

After the primary batch reaction was terminated, the  
20 reactor was stirred at the same temperature for one hour and then maintained at an internal temperature of 40°C. Then, 162 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 229.5 g of methyl methacrylate and 40.5 g of  
25 butyl acrylate in a ratio of 85:15 were added to the



reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution  
5 as used for the primary batch reaction were added to the reactor to perform a secondary batch reaction.

After the secondary batch reaction was terminated, the reactor was further stirred for 1.5 hours and then maintained at an internal temperature of 40°C. Then, 162 g  
10 of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 229.5 g of methyl methacrylate and 40.5 g of butyl acrylate in a ratio of 85:15 were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal  
15 temperature of 40°C under a nitrogen atmosphere and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as used for the primary batch reaction were added to the reactor to perform a tertiary batch reaction.

20 After the tertiary batch reaction was terminated, the reactor was further stirred for one hour to give a latex acrylic copolymer. The latex acrylic copolymer was subjected to coagulation with calcium chloride, dehydration, and drying, to give a powdery acrylic copolymer.

25 Main components used in each reaction process for the

preparation of the acrylic copolymer of Example 1 and acrylic copolymers of Examples 2-10 and Comparative Examples 1-7 as will be described later are summarized in Table 1 below.

5

(2) Measurement of degree of swelling and weight average molecular weight of acrylic copolymer

0.3 g of the powdery acrylic copolymer as prepared in Section (1) was dissolved in 100 ml of tetrahydrofuran (THF) for 50 hours and centrifuged at 16,000 rpm for 2 hours. After the centrifugation, a swelled gel and a sol were separated to measure the weight of the swelled gel. The swelled gel was then dried to measure the weight of the dried gel. The degree of swelling of the powdery acrylic copolymer was calculated according to the following Equation 1 and the result is presented in Table 2 below:

[Equation 1]

Degree of swelling = weight of swelled gel / weight of dried gel

20

Furthermore, the weight average molecular weight of the sol of the acrylic copolymer was measured using gel permeation chromatography (GPC) and the result is presented in Table 2 below. The weight average molecular weight of the acrylic copolymer except the crosslinked polymer

component was 4,300,000.

[Example 2]

An acrylic copolymer was prepared in the same manner  
5 as in Example 1 except that ethyl acrylate was used in the  
primary batch reaction, instead of the butyl acrylate. The  
degree of swelling and weight average molecular weight of  
the acrylic copolymer were measured and the results are  
presented in Table 2 below.

10

[Example 3]

An acrylic copolymer was prepared in the same manner  
as in Example 1 except that 59.5 g of a monomer mixture  
prepared by mixing ethyl acrylate and butyl acrylate in a  
15 ratio of 1:1 was used in the primary batch reaction,  
instead of 59.5 g of the butyl acrylate. The degree of  
swelling and weight average molecular weight of the acrylic  
copolymer were measured and the results are presented in  
Table 2 below.

20

[Example 4]

An acrylic copolymer was prepared in the same manner  
as in Example 1 except that a monomer mixture prepared by  
mixing 216 g of methyl methacrylate and 54 g of butyl  
25 acrylate in a ratio of 80:20 was used in the secondary and

tertiary batch reactions. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

5

[Example 5]

532 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 216 g of methyl methacrylate and 54 g of butyl acrylate in a ratio of 80:20 were placed in a 3l four-necked flask reactor equipped with a stirrer, a thermocouple, a nitrogen inlet, and a reflux condenser, to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as in Example 1 were added to the reactor to perform a primary batch reaction.

After the primary batch reaction was terminated, the reactor was stirred at the same temperature for one hour. Then, 50 g of ion exchange water, 10 g of a 8% potassium salt solution of fatty acid, 59.5 g of butyl acrylate, and 0.5 g of aryl methacrylate were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 62°C under a nitrogen atmosphere

and 0.45 g of t-butyl hydroperoxide (10% diluted solution) and 12 g of the same activation solution as in Example 1 were added to the reactor to perform a secondary batch reaction.

5        After the secondary batch reaction was terminated, the reactor was further stirred for 1.5 hours and then maintained at an internal temperature of 40°C. Then, 162 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 216  
10 g of methyl methacrylate and 54 g of butyl acrylate in a ratio of 80:20 were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g  
15 of the same activation solution as in Example 1 were added to the reactor to perform a tertiary batch reaction.

After the tertiary batch reaction was terminated, the reactor was further stirred for one hour to give a latex acrylic copolymer. The latex acrylic copolymer was  
20 subjected to coagulation with calcium chloride, dehydration, and drying, to give a powdery acrylic copolymer. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

25        [Example 6]

532 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 216 g of methyl methacrylate and 54 g of butyl acrylate in a ratio of 80:20 were added to a 3 l four-necked flask reactor equipped with a stirrer, a thermocouple, a nitrogen inlet, and a reflux condenser, to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere, and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as in Example 1 were added to the reactor to perform a primary batch reaction.

After the primary batch reaction was terminated, the reactor was further stirred for 1.5 hours and maintained at an internal temperature of 40°C. Then, 162 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 216 g of methyl methacrylate and 54 g of butyl acrylate in a ratio of 80:20 were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere, and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as in Example 1 were added to the reactor to perform a secondary batch reaction.

After the secondary batch reaction was terminated, the reactor was further stirred for 1.5 hours. Then, 50 g

of ion exchange water, 10 g of a 8% potassium salt solution of fatty acid, 59.5 g of butyl acrylate, and 0.5 g of aryl methacrylate were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal  
5 temperature of 62°C under a nitrogen atmosphere and 0.45 g of t-butyl hydroperoxide (10% diluted solution) and 12 g of the same activation solution as in Example 1 were added to the reactor to perform a tertiary batch reaction.

After the tertiary batch reaction was terminated, the  
10 reactor was further stirred for one hour to give a latex acrylic copolymer. The latex acrylic copolymer was subjected to coagulation with calcium chloride, dehydration, and drying, to give a powdery acrylic copolymer. The degree of swelling and weight average molecular weight of  
15 the acrylic copolymer were measured and the results are presented in Table 2 below.

[Example 7]

An acrylic copolymer was prepared in the same manner  
20 as in Example 4 except that ethyl acrylate was used in the primary batch reaction, instead of the butyl acrylate. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

## [Example 8]

An acrylic copolymer was prepared in the same manner as in Example 4 except that 59.5 g of a monomer mixture prepared by mixing ethyl acrylate and butyl acrylate in a ratio of 1:1 was used in the primary batch reaction, instead of 59.5 g of the butyl acrylate. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

10

## [Example 9]

An acrylic copolymer was prepared in the same manner as in Example 4 except that 0.1 g of the t-butyl hydroperoxide (10% diluted solution) and 3.4 g of the activation solution were used in the secondary and tertiary batch reactions. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

20

## [Example 10]

An acrylic copolymer was prepared in the same manner as in Example 4 except that in the secondary and tertiary batch reactions, the internal temperature of the reactor was maintained at 35°C and 0.06 g of the t-butyl hydroperoxide (10% diluted solution) and 2.3 g of the

25



activation solution were used. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

5

[Comparative Example 1]

An acrylic copolymer was prepared in the same manner as in Example 1 except that aryl methacrylate as a crosslinking agent was not used in the primary batch  
10 reaction. The weight average molecular weight of the acrylic copolymer was measured by GPC using THF as a mobile phase and the result is presented in Table 2 below.

The weight average molecular weights of the acrylic copolymer of Comparative Example 1 and acrylic copolymers  
15 of Comparative Examples 2 and 7 as will be described later were measured by GPC using THF as a mobile phase.

[Comparative Example 2]

An acrylic copolymer was prepared in the same manner  
20 as in Example 5 except that aryl methacrylate as a crosslinking agent was not used in the secondary batch reaction. The weight average molecular weight of the acrylic copolymer was measured by GPC using THF as a mobile phase and the result is presented in Table 2 below.

25

## [Comparative Example 3]

An acrylic copolymer was prepared in the same manner as in Example 1 except that 58.5 g of butyl acrylate and 1.5 g of aryl methacrylate were used in the primary batch  
5 reaction. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

## [Comparative Example 4]

10 An acrylic copolymer was prepared in the same manner as in Example 1 except that 59.9 g of butyl acrylate and 0.1 g of aryl methacrylate were used in the primary batch reaction. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and  
15 the results are presented in Table 2 below.

## [Comparative Example 5]

An acrylic copolymer was prepared in the same manner as in Example 4 except that 26.78 g of butyl acrylate and  
20 0.22 g of aryl methacrylate were used in the primary batch reaction and a monomer mixture prepared by mixing 229.2 g of methyl methacrylate and 57.3 g of butyl acrylate in a ratio of 80:20 was used in the secondary and tertiary batch reactions. The degree of swelling and weight average  
25 molecular weight of the acrylic copolymer were measured and

the results are presented in Table 2 below.

[Comparative Example 6]

An acrylic copolymer was prepared in the same manner  
5 as in Example 4 except that 92.23 g of butyl acrylate and  
0.77 g of aryl methacrylate were used in the primary batch  
reaction and a monomer mixture prepared by mixing 202.8 g  
of methyl methacrylate and 50.7 g of butyl acrylate in a  
ratio of 80:20 was used in the secondary and tertiary batch  
10 reactions. The degree of swelling and weight average  
molecular weight of the acrylic copolymer were measured and  
the results are presented in Table 2 below.

[Comparative Example 7]

15 420 g of ion exchange water, 10 g of a 8% potassium  
salt solution of fatty acid, 51 g of methyl methacrylate,  
and 9 g of butyl acrylate were placed in a 3l four-necked  
flask reactor equipped with a stirrer, a thermocouple, a  
nitrogen inlet, and a reflux condenser, to prepare an  
20 emulsion. Then, the reactor was maintained at an internal  
temperature of 62°C under a nitrogen atmosphere and 0.45 g  
of t-butyl hydroperoxide (10% diluted solution) and 12 g of  
the same activation solution as in Example 1 were added to  
the reactor to perform a primary batch reaction.

25 After the primary batch reaction was terminated, the

reactor was stirred at the same temperature for one hour and then adjusted to an internal temperature of 40°C. Then, 162 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 229.5 g of methyl methacrylate and 40.5 g of butyl acrylate in a ratio of 85:15 were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere, and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as in Example 1 were added to the reactor to perform a secondary batch reaction.

After the secondary batch reaction was terminated, the reactor was further stirred for 1.5 hours and then adjusted to an internal temperature of 40°C. Then, 162 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 229.5 g of methyl methacrylate and 40.5 g of butyl acrylate in a ratio of 85:15 were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere, and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as in Example 1 were added to the reactor to perform a tertiary batch reaction.

After the tertiary batch reaction was terminated, the

reactor was further stirred for one hour to give a latex acrylic copolymer. The latex acrylic copolymer was subjected to coagulation with calcium chloride, dehydration, and drying, to give a powdery acrylic copolymer. The weight average molecular weight of the powdery acrylic copolymer was measured by GPC using THF as a mobile phase and the result is presented in Table 2 below.

Examples 11-20 and Comparative Examples 8-14:

10 Preparation of vinyl chloride resins with good foaming property using acrylic copolymers

[Example 11]

(1) Preparation of vinyl chloride resin modified by acrylic copolymer (with filler)

15 6.4 g of a composite stabilizer KD-105 (Dansuk Industrial Co., Ltd.) prepared by uniformly mixing a thermal stabilizer and a lubricant, which is used as both a thermal stabilizer and a foam stabilizer, and 14 g of a filler ( $\text{CaCO}_3$ ) were added to 100 g of a vinyl chloride  
20 resin (LS080, LG Chemical, Co., Ltd.). Then, 5 g of the acrylic copolymer prepared in Example 1 and 0.8 g of azodicarbonamide were added and mixed by a Henschel mixer with heating to  $115^\circ\text{C}$  to prepare a vinyl chloride resin modified with the acrylic copolymer.

(2) Measurement of melt time of vinyl chloride resin

64 g of the vinyl chloride resin prepared in Section (1) was mixed at 180°C and 40 rpm in a Brabender. Then, a melt time defined as a time required from minimum load to maximum load was measured and is presented in Table 2 below.

(3) Evaluation of foaming property of vinyl chloride resin

The vinyl chloride resin prepared in Section (1) was extruded in the form of a rectangular rod of 5 mm (thickness) × 30 mm (width) using a 30 mm single spindle extruder equipped with a rectangular slit die at a cylinder temperature of 180°C and a screw speed of 30 rpm and then cut into length of 5 mm. The foam density of the foamed products thus obtained was measured using a gravimeter and the result is presented in Table 2 below. As the foam density decreases, foaming property is good.

Meanwhile, based on an expansion ratio defined as the ratio (a/b) of the foam density (a) of a foamed product with no acrylic copolymer to the foam density (b) of a foamed product with acrylic copolymer, the expansion ratio of the foamed products of this Example was calculated and the result is presented in Table 2 below.

In addition, the sections of the foamed products were observed with an optical microscope. Scoring criteria were

as follows: 5 = uniform foamed cells, 3 = slightly non-uniform foamed cells, and 1 = non-uniform foamed cells. The results are presented in Table 2 below.

5        (4) Preparation of vinyl chloride resin modified by acrylic copolymer (with no filler)

A vinyl chloride resin was prepared in the same manner as in Section (1) except that no fillers were used.

10       (5) Measurement of fish-eyes in vinyl chloride resin

The vinyl chloride resin prepared in Section (4) was extruded in the form of 0.2 mm thickness film using a 20 mm single spindle extruder equipped with a T-die at a cylinder temperature of 180°C and screw speed of 30 rpm and then the number of fish-eyes present in a predetermined surface region of the film was counted with a naked eye. Scoring criteria were as follows: 5 = few fish-eyes, 3 = a few fish-eyes, and 1 = many fish-eyes. The evaluation result is presented in Table 2 below.

20

[Example 12]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Example 2. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and

the evaluation results are presented in Table 2 below.

[Example 13]

A vinyl chloride resin was prepared in the same  
5 manner as in Example 11 using the acrylic copolymer of  
Example 3. The melt time, foaming property, and the number  
of fish-eyes of the vinyl chloride resin were evaluated and  
the evaluation results are presented in Table 2 below.

10 [Example 14]

A vinyl chloride resin was prepared in the same  
manner as in Example 11 using the acrylic copolymer of  
Example 4. The melt time, foaming property, and the number  
of fish-eyes of the vinyl chloride resin were evaluated and  
15 the evaluation results are presented in Table 2 below.

[Example 15]

A vinyl chloride resin was prepared in the same  
manner as in Example 11 using the acrylic copolymer of  
20 Example 5. The melt time, foaming property, and the number  
of fish-eyes of the vinyl chloride resin were evaluated and  
the evaluation results are presented in Table 2 below.

[Example 16]

25 A vinyl chloride resin was prepared in the same



manner as in Example 11 using the acrylic copolymer of Example 6. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

5

[Example 17]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Example 7. The melt time, foaming property, and the number  
10 of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

[Example 18]

A vinyl chloride resin was prepared in the same  
15 manner as in Example 11 using the acrylic copolymer of Example 8. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

20

[Example 19]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Example 9. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and  
25 the evaluation results are presented in Table 2 below.

## [Example 20]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Example 10. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

## 10 [Comparative Example 8]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Comparative Example 1. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

## [Comparative Example 9]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Comparative Example 2. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

## [Comparative Example 10]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Comparative Example 3. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

## [Comparative Example 11]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Comparative Example 4. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

## [Comparative Example 12]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Comparative Example 5. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

## [Comparative Example 13]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Comparative Example 6. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

[Comparative Example 14]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Comparative Example 7. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

15

Table 1

Section	Main components (g) of each reaction		
	Primary reaction	Secondary reaction	Tertiary reaction
Exam. 1	Butyl acrylate (59.5) Aryl methacrylate (0.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)
Exam. 2	Ethyl acrylate (59.5) Aryl methacrylate (0.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)
Exam. 3	1:1 mixture of butyl acrylate and ethyl acrylate (59.5) Aryl methacrylate (0.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)
Exam. 4	Butyl acrylate (59.5) Aryl methacrylate (0.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Exam. 5	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Butyl acrylate (59.5) Aryl methacrylate (0.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Exam. 6	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Butyl acrylate (59.5) Aryl methacrylate (0.5)
Exam. 7	Ethyl acrylate (59.5) Aryl methacrylate (0.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Exam. 8	1:1 mixture of butyl acrylate and ethyl acrylate (59.5) Aryl methacrylate (0.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Exam. 9	Butyl acrylate (59.5) Aryl methacrylate (0.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Exam.10	Butyl acrylate (59.5) Aryl methacrylate (0.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Comp. 1	Butyl acrylate (59.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)
Comp. 2	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Butyl acrylate (59.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Comp. 3	Butyl acrylate (58.5) Aryl methacrylate (1.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)
Comp. 4	Butyl acrylate (59.9) Aryl methacrylate (0.1)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)
Comp. 5	Butyl acrylate (26.78) Aryl methacrylate (0.22)	Methyl methacrylate (229.2) Butyl acrylate (57.3)	Methyl methacrylate (229.2) Butyl acrylate (57.3)
Comp. 6	Butyl acrylate (92.23) Aryl methacrylate (0.77)	Methyl methacrylate (202.8) Butyl acrylate (50.7)	Methyl methacrylate (202.8) Butyl acrylate (50.7)
Comp. 7	Methyl methacrylate (51.0) Butyl acrylate (9.0)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)

Exam.: Example, Comp.: Comparative Example

Table 2

Section	Degree of swelling	WAMW (x10,000)	Section	Melt time (s)	Fish eye	Foaming property		
						Foam density (g/cm <sup>3</sup> )	Expansion ratio	Uniformity of foamed cells
Exam. 1	6.1	430	Exam. 11	93	4.0	0.72	1.65	4.5
Exam. 2	6.6	410	Exam. 12	89	4.0	0.73	1.63	4.0
Exam. 3	6.3	410	Exam. 13	92	4.0	0.73	1.63	4.5
Exam. 4	6.2	420	Exam. 14	90	5.0	0.71	1.68	4.5
Exam. 5	5.9	410	Exam. 15	88	5.0	0.72	1.65	4.0
Exam. 6	5.6	410	Exam. 16	88	4.0	0.73	1.63	4.0
Exam. 7	6.1	410	Exam. 17	88	5.0	0.73	1.63	4.0
Exam. 8	6.5	420	Exam. 18	90	5.0	0.74	1.61	4.5
Exam. 9	6.0	650	Exam. 19	93	5.0	0.68	1.75	5.0
Exam. 10	5.8	910	Exam. 20	95	5.0	0.67	1.78	5.0
Comp. 1	-	400	Comp. 8	90	5.0	0.79	1.51	3.0
Comp. 2	-	410	Comp. 9	88	5.0	0.77	1.55	3.0
Comp. 3	2.3	420	Comp. 10	89	4.0	0.79	1.51	3.0
Comp. 4	11.2	440	Comp. 11	85	4.0	0.72	1.65	3.0
Comp. 5	6.2	450	Comp. 12	87	5.0	0.79	1.51	3.5
Comp. 6	6.4	400	Comp. 13	92	4.0	0.73	1.63	3.0
Comp. 7	-	400	Comp. 14	98	4.0	0.82	1.45	4.0

Exam.: Example, Comp.: Comparative Example, WAMW: weight average molecular weight

5

As shown in Table 2, the vinyl chloride resins of Examples 11-20 prepared using the acrylic copolymers of Examples 1-10 in which a crosslinked polymer was prepared from aryl methacrylate as a crosslinking agent and alkyl acrylate, exhibited superior foam density, expansion ratio, and uniformity of foamed cells, as compared to the vinyl

chloride resins of Comparative Examples 8 and 9 prepared using the acrylic copolymers of Comparative Examples 1 and 2 in which no crosslinked polymers were prepared due to the absence of a crosslinking agent such as aryl methacrylate.

5        Furthermore, the vinyl chloride resin of Comparative Example 10 prepared using the acrylic copolymer of Comparative Example 3 having the degree of swelling of 2.3 exhibited poor die swell property, thereby lowering an expansion ratio, as compared to the vinyl chloride resins  
10 of Examples 11-20 prepared using the acrylic copolymers of Examples 1-10 having the degree of swelling of 3 to 10. The vinyl chloride resin of Comparative Example 11 prepared using the acrylic copolymer of Comparative Example 4 having the degree of swelling of 11.2 exhibited a high expansion  
15 ratio but poor processability, thereby lowering foaming properties.

      The vinyl chloride resin of Comparative Example 12 prepared using the acrylic copolymer of Comparative Example 5, in which the content of alkyl acrylate and a  
20 crosslinking agent was 4.5 wt% per the total weight of all the monomers used in the preparation of the acrylic copolymer, exhibited a low expansion ratio, resulting in a poor foamed product. On the other hand, the vinyl chloride resin of Comparative Example 13 prepared using the acrylic  
25 copolymer of Comparative Example 6, in which the content of

alkyl acrylate and a crosslinking agent was 15.5 wt% per the total weight of all the monomers used in the preparation of the acrylic copolymer, produced non-uniform foamed cells.

5       The vinyl chloride resin of Comparative Example 14 prepared using the acrylic copolymer of Comparative Example 7, in which no crosslinked polymer was prepared due to the absence of a crosslinking agent such as aryl methacrylate, produced a foamed product with low expansion ratio.

10       The vinyl chloride resins of Examples 19 and 20 prepared using the acrylic copolymers of Examples 9 and 10 exhibited an increased melt strength due to the high molecular weight of the acrylic copolymers, resulting in uniform foamed cells.

15       From the above Examples and Comparative Examples, it can be seen that when an acrylic copolymer contains a crosslinked polymer with a predetermined swelling degree and has a high molecular weight, foaming property is enhanced. This is because the vinyl chloride resins of  
20 Examples have good melt strength and die swell property, thereby ensuring a low foam density and uniform foamed cells, as compared to those of Comparative Examples.

Examples 21-26 and Comparative Examples 15-17:

25 Preparation of vinyl chloride resins with good impact



strength using acrylic copolymers

[Example 21]

(1) Preparation of acrylic impact modifier

5        415.8 g of ion exchange water was added to a reactor which was then heated to 78°C with nitrogen washing. When the ion exchange water reached 78°C, 43.56 g of butyl acrylate, 0.72 g of 1,3-butanediol diacrylate, 0.72 g of methacrylic acid, and 24.21 g of 8 % potassium salt  
10 solution of fatty acid were at a time added to the reactor. While the internal temperature of the reactor was maintained at 78°C, a seed reaction was carried out by addition of 12.6 g of 3% potassium persulfate solution to prepare a rubber latex. The nitrogen washing was continued  
15 until the seed reaction was terminated.

276.45 g of the rubber latex prepared by the seed reaction and 9.37 g of 8% potassium salt solution of fatty acid were sequentially added to a reactor which was then heated to 78°C with nitrogen washing and stirred at 15°C to  
20 obtain a pre-emulsion. Then, a mixture of 180.3 g of ion exchange water, 288.9 g of butyl acrylate, 0.35 g of 1,3-butanediol diacrylate, 0.75 g of aryl methacrylate, 34.67 g of 8% potassium salt solution of fatty acid, and 8.33 g of 3% potassium persulfate solution was added to the reactor  
25 to perform a primary core reaction. The reactor was

maintained at 78°C and the nitrogen washing was continued until the core reaction was terminated.

A mixture of 59.2 g of ion exchange water, 109.2 g of butyl acrylate, 0.15 g of 1,3-butanediol diacrylate, 0.65 g of aryl methacrylate, 15.62 g of 8% potassium salt solution of fatty acid, and 6.67 g of 3% potassium persulfate solution was stirred to obtain a pre-emulsion. The pre-emulsion was added to the reactor containing a product of the primary core reaction using a pump for one hour to perform a secondary core reaction and then incubated for one hour. The reactor was maintained at 78°C and nitrogen washing was continued until the secondary core reaction was terminated.

A mixture of 97.4 g of ion exchange water, 71.25 g of methyl methacrylate, 3.75 g of ethyl acrylate, 2.8 g of acrylonitrile, 9.37 g of 8% potassium salt solution of fatty acid, and 6.33 g of 3% potassium persulfate solution was sufficiently stirred to obtain a pre-emulsion. The pre-emulsion was added to the reactor for 1.5 hours to perform a shell reaction, and then incubated for one hour. The reactor was maintained at 78°C and nitrogen washing was continued until the shell reaction was terminated. As a result, a latex acrylic impact modifier was obtained. The latex acrylic impact modifier was subjected to coagulation with calcium chloride, dehydration, and drying, to give a

powdery acrylic impact modifier.

(2) Preparation of mixture of impact modifier and acrylic copolymer

5        90 g of the powdery acrylic impact modifier prepared in Section (1) and 10 g of the powdery acrylic copolymer prepared in Example 4 were mixed by a Henschel mixer with heating to 100°C to prepare a mixture of the impact modifier and the acrylic copolymer.

10

(3) Preparation of vinyl chloride resin modified by impact modifier and acrylic copolymer

100 g of a vinyl chloride resin (LS-100, LG Chemical Co., Ltd.), 2.0 g of a tin-based thermal stabilizer, BT-107,  
15 1.2 g of calcium stearate (Ca-St), 1.0 g of polyethylene wax (PE Wax), 1.5 g of a processing aid (PA822, LG Chemical Co., Ltd.), 14 g of a filler (CaCO<sub>3</sub>), and 6 g of the mixture of the impact modifier and the acrylic copolymer prepared in Section (2) were mixed by a Henschel mixer with  
20 heating to 115°C to give a modified vinyl chloride resin.

(4) Measurement of extrusion output of vinyl chloride resin modified by impact modifier and acrylic copolymer

The vinyl chloride resin prepared in Section (3) was  
25 extruded by a twin screw extruder under processing

temperature conditions of 170°C, 180°C, 185°C, and 190°C. A hot extrudate drawn away from a capillary die exit with diameter of 0.635 cm was cut into length of 0.8 cm to obtain extrudate pieces. The weights of three collections  
5 of the extrudate pieces were measured and averaged (?). The result is presented in Table 3 below.

(5) Charpy impact strength test of vinyl chloride resin modified by impact modifier and acrylic copolymer

10 The vinyl chloride resin prepared in Section (3) was milled by 2-roll mill at 190°C for 7 minutes to obtain 0.6mm sheets. The sheets were cut into size of 150mm×200mm and laminated in a predetermined milling direction on molds of 3mm×170mm×220mm. The resultant  
15 laminates were preheated by a 195°C heating press for 8 minutes (0.5 kg), pressed for 2 minutes (10 kg), and cooled for 3 minutes (10 kg) to obtain 3 mm-thickness specimens. The impact strength of the specimens was measured at 23°C and -10°C according to ASTM D-256  
20 standard and the result is presented in Table 3 below.

(6) Measurement of melt time of vinyl chloride resin modified by impact modifier and acrylic copolymer

The melt time of the vinyl chloride resin of Section  
25 (3) was measured in the same manner as in Example 11 and

the result is presented in Table 3 below.

[Example 22]

A vinyl chloride resin was prepared in the same  
5 manner as in Example 21 except that 85 g of the powdery  
acrylic impact modifier prepared in Section (1) of Example  
21 and 15 g of the powdery acrylic copolymer prepared in  
Example 4 were used. The extrusion output, impact strength,  
and melt time of the vinyl chloride resin were measured and  
10 the results are presented in Table 3 below.

[Example 23]

A vinyl chloride resin was prepared in the same  
manner as in Example 21 except that 80 g of the powdery  
15 acrylic impact modifier prepared in Section (1) of Example  
21 and 20 g of the powdery acrylic copolymer prepared in  
Example 4 were used. The extrusion output, impact strength,  
and melt time of the vinyl chloride resin were measured and  
the results are presented in Table 3 below.

20

[Example 24]

A vinyl chloride resin was prepared in the same  
manner as in Example 21 except that 208.40 g of the latex  
acrylic impact modifier prepared in Section (1) of Example  
25 21 and 23.61 g of the latex acrylic copolymer prepared in

Example 4 were mixed followed by coagulation with calcium chloride, dehydration, and drying. The extrusion output, impact strength, and melt time of the vinyl chloride resin were measured and the results are presented in Table 3 below.

[Example 25]

A vinyl chloride resin was prepared in the same manner as in Example 21 except that 196.82 g of the latex acrylic impact modifier prepared in Section (1) of Example 21 and 35.41 g of the latex acrylic copolymer prepared in Example 4 were mixed followed by coagulation with calcium chloride, dehydration, and drying. The extrusion output, impact strength, and melt time of the vinyl chloride resin were measured and the results are presented in Table 3 below.

[Example 26]

A vinyl chloride resin was prepared in the same manner as in Example 21 except that 185.25 g of the latex acrylic impact modifier prepared in Section (1) of Example 21 and 47.22 g of the latex acrylic copolymer prepared in Example 4 were mixed followed by coagulation with calcium chloride, dehydration, and drying. The extrusion output, impact strength, and melt time of the vinyl chloride resin

were measured and the results are presented in Table 3 below.

[Comparative Example 15]

5        A vinyl chloride resin was prepared in the same manner as in Example 21 except that 95 g of the powdery acrylic impact modifier prepared in Section (1) of Example 21 and 5 g of the powdery acrylic copolymer prepared in Example 4 were used. The extrusion output, impact strength,  
10 and melt time of the modified vinyl chloride resin were measured and the results are presented in Table 3 below.

[Comparative Example 16]

15        A vinyl chloride resin was prepared in the same manner as in Example 21 except that 70 g of the powdery acrylic impact modifier prepared in Section (1) of Example 21 and 30 g of the powdery acrylic copolymer prepared in Example 4 were used. The extrusion output, impact strength, and melt time of the vinyl chloride resin were measured and  
20 the results are presented in Table 3 below.

[Comparative Example 17]

25        A vinyl chloride resin was prepared in the same manner as in Example 21 except that 100 g of the powdery acrylic impact modifier prepared in Section (1) of Example

21 was used in the absence of the acrylic copolymer prepared in Example 4. The extrusion output, impact strength, and melt time of the vinyl chloride resin were measured and the results are presented in Table 3 below.

5



Table 3

Section		Phase of acrylic copolymer and impact modifier mixture	Acrylic copolymer (wt%)	Impact modifier (wt%)	Extrusion output (g)	Impact strength (kgcm/cm)		Melt time (sec.)
						23℃	-10℃	
Example	21	Powder	10	90	1.07	26.8	8.1	102
	22	Powder	15	85	1.09	27.5	8.3	94
	23	Powder	20	80	1.15	29.1	8.6	90
	24	Latex	10	90	1.05	27.1	8.2	105
	25	Latex	15	85	1.07	28.3	8.5	89
	26	Latex	20	80	1.12	28.9	8.7	90
Comparative Example	15	Powder	5	95	1.02	22.4	6.9	110
	16	Powder	30	70	1.17	21.9	7.1	76
	17	Powder	-	100	0.95	22.4	7.6	121

As shown in Table 3, the vinyl chloride resins of Examples 21-26 prepared using a mixture comprising 5-30 wt% of an acrylic copolymer prepared according to the present invention and 70-95 wt% of an impact modifier exhibited excellent impact strength and processability, regardless of whether the impact modifier and the acrylic copolymer were mixed in a powder or latex phase. Here, the processability was evaluated by the extrusion output and the melt time. As the extrusion output increases, the processability increases. The melt time may vary according to used conditions. However, in view of foaming conditions, the melt time is preferably in a range of 80-110 seconds, and optimally 90 seconds. In this regard, the vinyl chloride

resin of Comparative Example 15, in which 95 parts by weight of the impact modifier and 5 parts by weight of the acrylic copolymer were used, did not sufficiently exhibit the processability of the acrylic copolymer, thereby  
5 lowering the processability of the vinyl chloride resin. The vinyl chloride resin of Comparative Example 16, in which 70 parts by weight of the impact modifier and 30 parts by weight of the acrylic copolymer were used, exhibited a low impact strength due to a counteractive  
10 effect of the acrylic copolymer on the impact modifier. The vinyl chloride resin of Comparative Example 17, in which only the impact modifier was used, exhibited very long melt time and poor processability that induces a non-uniform formed product, and low impact strength.

15

#### Industrial Applicability

As apparent from the above description, when an acrylic copolymer prepared by the method of the present invention is added to a vinyl chloride resin composition in  
20 a predetermined amount, the processability of the vinyl chloride resin can be enhanced, resulting in an excellent foamed product. Combination of the acrylic copolymer with an impact modifier can further enhance the impact strength of the vinyl chloride resin.

While the present invention has been particularly shown and described with reference to exemplary embodiments thereof, it will be understood by those of ordinary skill in the art that various changes in form and details may be made therein without departing from the spirit and scope of the present invention as defined by the following claims.